



# $\begin{array}{l} \textbf{RECENT DEVELOPMENTS IN ION MOLECULE} \\ \textbf{REACTION} - \textbf{MASS SPECTROMETRY} \\ \textbf{FOR CO}_2 \textbf{ QUALITY MONITORING} \end{array}$

#### Front Door to Back Door

#### BevTech'16, Ft. Myers

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And

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- IMR MS Technology using a *Dual Capillary* Inlet System
- Latest Applications
  - Final Product ISBT Purity Gas Monitoring
  - $\circ$  Catox Optimization
  - Fermentation Plant Feed- In-Process Final Product
  - Natural Well Feed Gas Profiles & GC Correlation
  - TSC Reductive Converter *Extended* Feed Gas Applications



# **Beverages / Foods / Packaging**

- CO<sub>2</sub>
- Beverages
- Food
- Flavors
- Flavors: good/bad breath + nose-space
- Mold in beverages, jelly
- PET Bottle Contamination
  - Monitoring



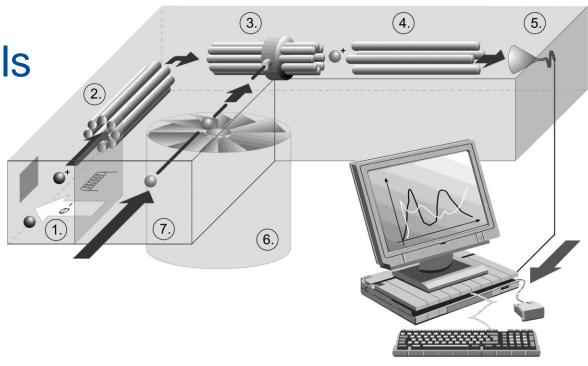


#### **IMR-MS** Technology

### Use of discrete energy levels

- LE: 10.44 eV
- ME: 12.13 eV
- HE: 13.99 eV

# followed by



Primary Ion Source
 Octopole Seperation Device

Charge Exchange Cell
 Quadrupole - Mass Filter
 Particle Detector

6. Vacuum System
 7. Gas Inlet System

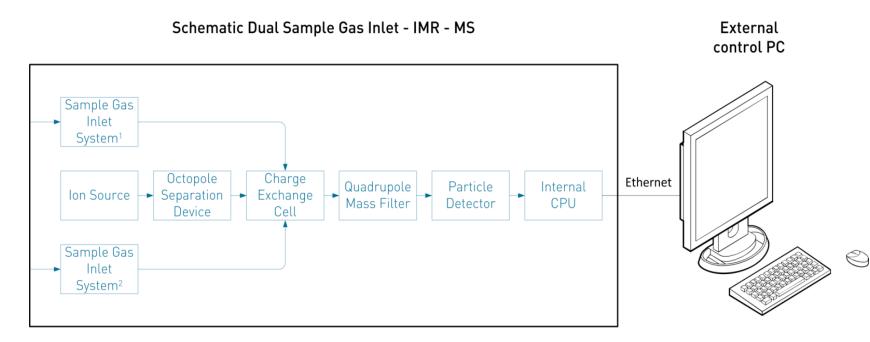
Ion Molecule Reaction with sample gas

molecules & <u>Mass Spectrometry = IMR - MS</u>





#### **IMR-MS Technology – Dual Capillary Inlet**





<sup>1</sup> Sample gas inlet for final CO<sub>2</sub> product quality

<sup>2</sup> Optional sample gas inlet for CO<sub>2</sub> feed- and process gas analysis



#### IMR-MS Technology

- Single two-body reactive collision conditions in charge exchange chamber
  - $\circ$  Neutral, purely kinetic collisions  $\rightarrow$  no change of ion mass number
  - $\circ$  Very low operating pressure → long mean free path between particles → Avoidance of bulk gas ionization
- Simultaneous detection of organic and inorganic compounds resp. compound classes (online or offline)
- Concentrations: ppt ppb ppm Vol%
- Time of analysis: > 1 msec per compound



#### **IMR-MS** Technology - CO<sub>2</sub> Applications

#### Feed Gas

- Sources: combustion, natural wells, fermentation, geothermal emission, ammonia, coal gasification, ethylene oxide, phosphate rocks, etc.
- $\circ$  CO<sub>2</sub> Impurities: ppb Vol %
- Online monitoring of impurity profiles
  & time variations

#### In-Process

 $\circ$  Online monitoring of CO<sub>2</sub> purification steps of catox, hydrocat, hydrolyzer, carbon beds, scrubbers, filters, etc.

#### Final Product Quality Control

Product to Storage, Storage Tanks, Truck filling stations











**IMR-MS Technology – Catox Monitoring Applications** 

#### • CO<sub>2</sub> Feed Gas - Petrochemical Plant – Background:

- $\,\circ\,$  Catox malfunction in contrast to its design specs
- $_{\odot}$  Time-Related decrease in Catox conversion rate
- Regeneration of Catox activity at lower temperatures
- $\circ$  Breakthrough of small organics in the CO<sub>2</sub> feed gas
- $\circ$  IMR-MS Monitoring of major impurities: O<sub>2</sub>, H<sub>2</sub>O, methane, ethylene, propylene, acetaldehyde, ethylene oxide, etc.



#### **A.** Original CATOX: 0.3% Pt on $AI_2O_3$

- T-in Catox from 390 360 C: 1.5 7.5 ppm ethylene (maximum desired value: 1 ppm)
- $\circ$  Addition of adsorbent  $\rightarrow$  no better performance
- Possible solution: higher operating Catox temperature
- $\circ$  Catalytic oxidation: exothermal  $\rightarrow$  too high temperature  $\rightarrow$  high risk for damage of Catox



#### B. New Catox: 0.15% Pt + 0.15% Pd on Al2O3

• At T-in 360 – 380 C: worse performance than original Catox

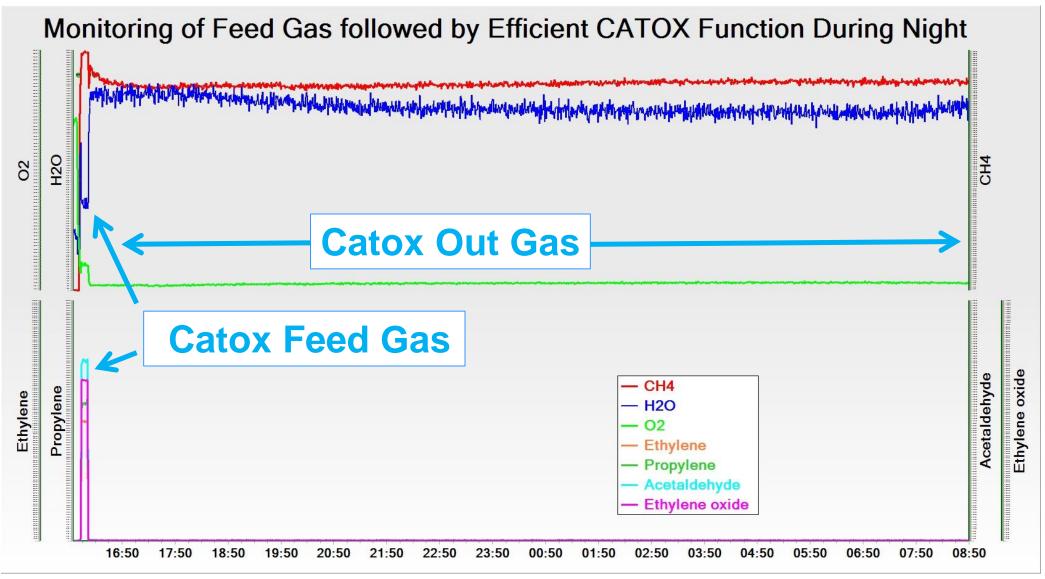
 $\circ$  At T-in > 430 C: better performance than original Catox

#### Solution:

Installation of *1st layer* of original Pt catalyst + *2nd layer* of Pt + Pd catalyst with appropriate gas hourly space velocity



#### **IMR-MS Technology – Catox Monitoring Applications**





#### **IMR-MS Technology – Fermentation Plant In-Process Monitoring**

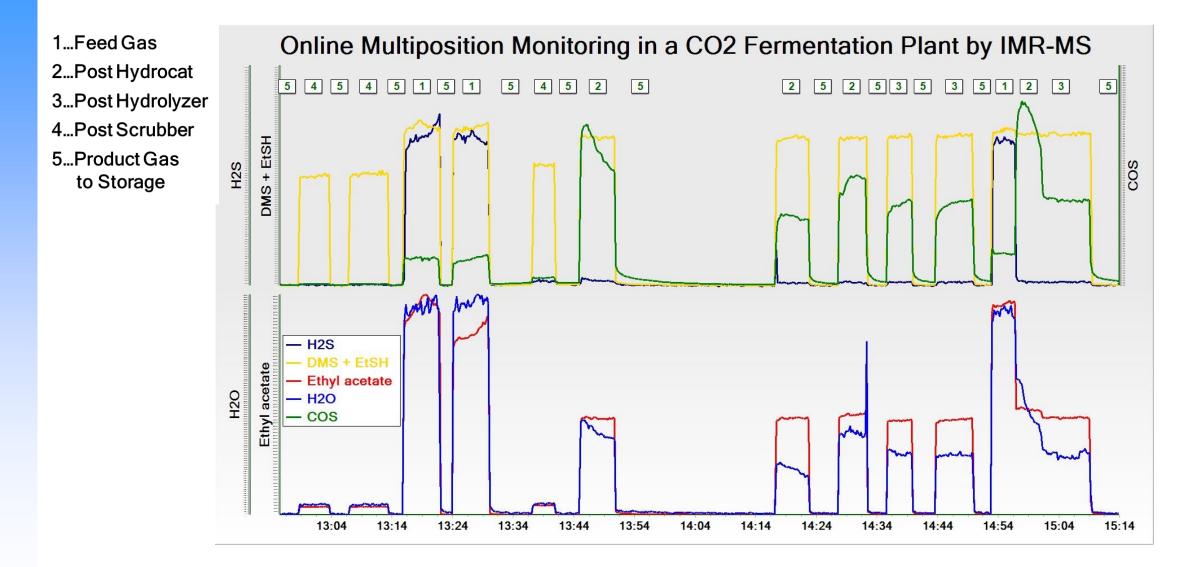
- In-Process Monitoring @ Key locations
  <u>Requirements</u>
  - Fast respond to process & concentration
    changes from Feed Gas In-Process Final Product
  - Rapid Sample location switching.



- Adequate temperatures of wet gas streams
- $\,\circ\,$  Regulated / equal pressures & flow rate for each sample location



#### **IMR-MS Technology – Fermentation Plant In-Process Monitoring**





#### IMR-MS Technology – Natural Well Monitoring vs GC Data

Compounds	GC Result	IMR-MS Result	Difference GC vs. IMR-MS [%]
Methane [ppm]	3,100	3,140	1.3
Ethane [ppm]	1,200	1,300	8.3
Propylene [ppm]	0.20	0.23	15.0
Benzene [ppb]	18	15	-16.7
Toluene [ppb]	4,310	4,310	0.0
Hydrogen Sulfide [ppm]	0.54	0.54	0.0
Carbonyl Sulfide [ppm]	1.7	1.4	-17.6



#### **Background & Definitions**

#### **Total Sulfur Converter**

- It is important to monitor Total Sulfur Content (TSC) in both feed and final product  $CO_2$ .
- $\circ$  TSC is present in most CO<sub>2</sub> feed gas sources.
- High TSC has caused many beverage recalls.
- Unexpected increases of TSC in feed gas can cause liquid  $CO_2$  quality upsets.
- Most on-line analyzers do not have the wide measurement range and H<sub>2</sub>O tolerance for single instrument TSC analysis for both feed gas and final product.

ISBT Bulk Carbon Dioxide Quality Guidelines and Analytical Methods Reference 2010 (Method 13.0, recommends a TSC Limit = 0.1 ppm v/v (IMR-MS [SIS] is an acceptable method for this application)







#### **Background & Definitions**

Carbonyl Sulfide (COS) is the most important Volatile Sulfur Compound to monitor.

- COS is odorless.
- COS can be created during the CO<sub>2</sub> manufacturing process and is very common in feed gas sources.
- COS slowly hydrolyses into highly odiferous H<sub>2</sub>S (rotten eggs smell) in acidic conditions such as carbonated beverages.
- High COS is historically responsible for most sulfur related odor complaints and packaged beverage recalls.

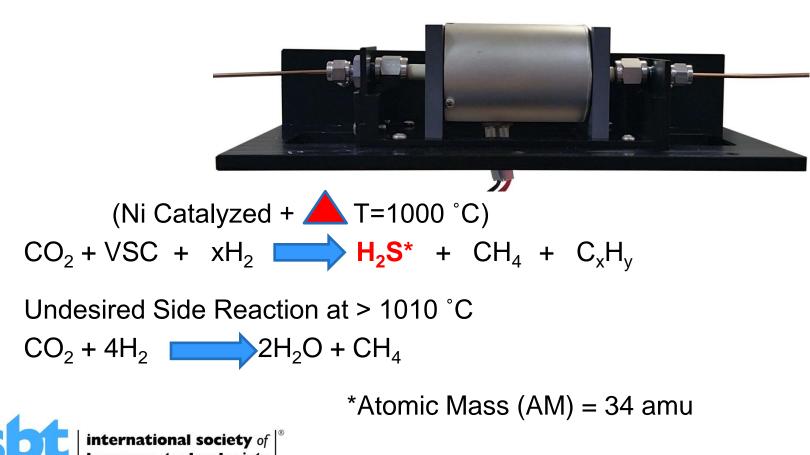




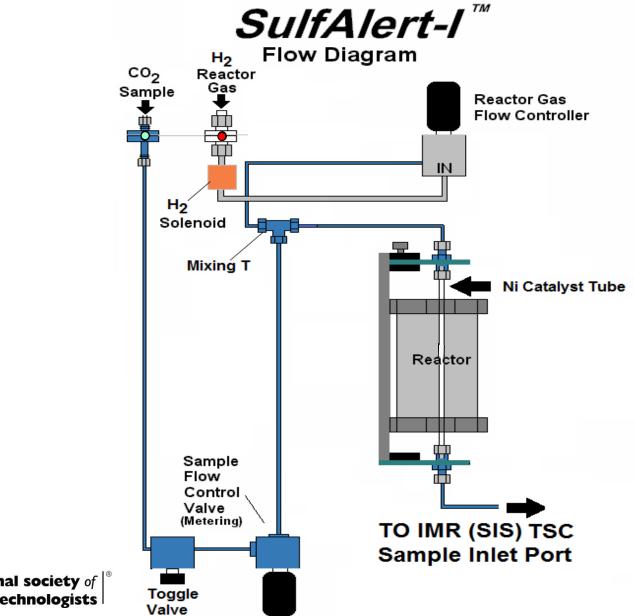
#### **Background & Definitions**

**TSC Objective:** ISBT Method 13.0 – Convert all forms of Volatile Sulfur Compounds (VSC) in  $CO_2$ , into a single form for measurement as Total Sulfur Content. This can be achieved by either a reductive or oxidative conversion.

#### **Reductive TSC Reactor**



#### **TSC-SIS Hardware / Plumbing**



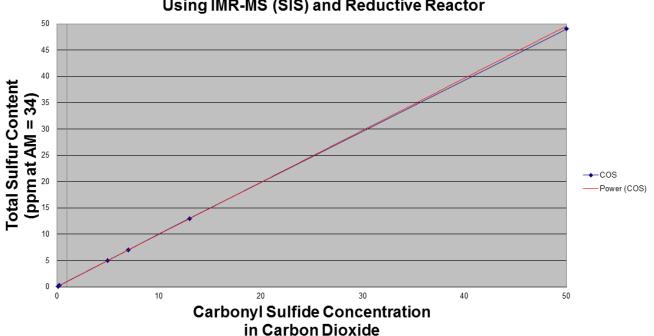
- Sample
- Hydrogen
- Total Sulfur



#### **TSC Performance Data**

#### **TSC Measurement Range**

- ISBT Method 13.0 recommended working range: 0.00 – 1 ppm v/v
   Limits: 0.1 ppm v/v TSC and 1.0 ppm v/v SO<sub>2</sub>.
- Current range is 0.00 ppm v/v to ≈50 ppm v/v\*.
- Most commercial feed gas sources have TSC < 50 ppm.</li>



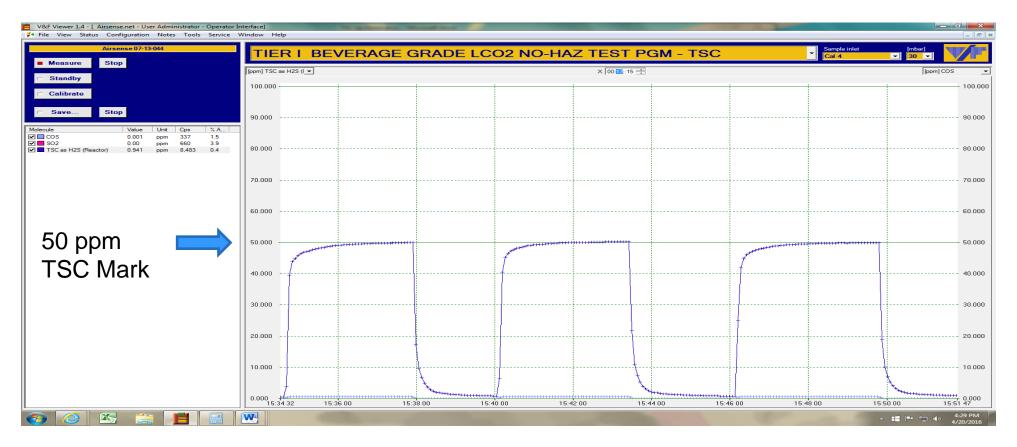
Conversion of COS to TSC Using IMR-MS (SIS) and Reductive Reactor

\* Higher ranges not studied to date.



#### **TSC Performance Data**

#### **TSC Measurement @ 50 ppm Level**



Alternating analysis from 50 ppm COS to Zero CO<sub>2</sub>

% COS conversion to TSC  $\approx$  98+%



#### Key Sulfur Species currently being Studied at Feed Gas Impurity Levels

- Carbonyl Sulfide (COS)
- Hydrogen Sulfide (H<sub>2</sub>S)
- Dimethyl Sulfide (DMS)
- Ethyl Mercaptan (EtSH)
- Carbon Disulfide  $(CS_2)$
- Sulfur Dioxide (SO<sub>2</sub>)

#### Advantage:

 Both TSC & speciated VSC are *simultaneously* monitored by the IMR-MS (SIS) with TSC reactor outlet.



#### Summary

IMR-MS (SIS) analyzers equipped with dual capillary inlets and reductive TSC converters exhibit a wide measurement range which is required for:

- Continuous CO<sub>2</sub> feed gas monitoring.
- Continuous in-process CO<sub>2</sub> composition.
- Continuous monitoring of beverage grade CO<sub>2</sub> for TSC and other key parameters.











# **Questions?**

# Thank you for your Interest!

